

Thermodynamic investigations of excess heat capacities of ternary liquid mixtures containing [Bmmim][BF₄] + [Bmim][BF₄] or [Emim][BF₄] + cyclopentanone or cyclohexanone

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Abstract In this paper, molar heat capacities (C_p)₁₂₃ data of 1-butyl-2,3-dimethylimidazolium tetrafluoroborate, [Bmmim][BF₄] (1) + 1-butyl-3-methylimidazolium tetrafluoroborate, [Bmim][BF₄] or 1-ethyl-3-methylimidazolium tetrafluoroborate, [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures have been reported over the entire range of composition at (293.15, 298.15, 303.15, 308.15) K using micro-differential scanning calorimeter (Model— μ DSC 7 Evo). The results have been utilized to calculate excess heat capacities (C_p^E)₁₂₃ values of the studied mixtures. The (C_p^E)₁₂₃ data have been fitted to Redlich–Kister equation to obtain ternary coefficients and standard deviations. The Moelwyn–Huggins concept of interaction between the surfaces of constituents of binary mixtures (Huggins in J Phys Chem 74:371–378, 1970) containing ionic liquid as one of the component has been extended to obtain expression (Graph theory) for (C_p^E)₁₂₃ of ternary mixtures. The comparison between experimental and estimated values (Graph theory) suggests that while 1-butyl-2,3-dimethylimidazolium tetrafluoroborate or 1-butyl-3-methylimidazolium tetrafluoroborate or 1-ethyl-3-methylimidazolium tetrafluoroborate exists as monomer, cyclopentanone or cyclohexanone exists as mixture of open and cyclic dimer. The results further support the various processes involved in the formation of present mixtures. The (C_p^E)₁₂₃ values have also been tested in term of modified Flory’s theory.

Keywords 1-butyl-2,3-dimethylimidazolium tetrafluoroborate · Micro-DSC · Excess heat capacities · (C_p^E)₁₂₃, connectivity parameter of third degree · ${}^3\zeta$, interaction energy parameter, χ

Introduction

Thermodynamic properties of liquid mixtures have great importance in theoretical and applied areas of research. The knowledge of these properties is frequently used in the design processes like flow, mass transfer or heat transfer calculations of many chemical and industrial processes [1–3]. Also these properties of liquid mixtures represent a useful complementary tool to extract the information about the structural features of the constituents of the mixture in pure as well as mixed state. The molar heat capacity, C_p , of a substance is a basic pure component property which plays a central role in all processes involving the uptake, release or transfer of heat energy and thus can be utilized for many engineering calculations [4–6]. Molar heat capacities, C_p , and excess heat capacities, C_p^E , of liquid mixtures are most needed properties in the design as well as optimization of the industrial processes such as food processing, estimation of heating or cooling requirements, heat storage capacity and also of equipment in the part where heat transfer is important [7–10].

In recent studies, excess heat capacities, C_p^E , of 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-butyl-3-methylimidazolium tetrafluoroborate or 1-ethyl-3-methylimidazolium tetrafluoroborate (2); 1-butyl-2,3-dimethylimidazolium tetrafluoroborate or 1-butyl-3-methylimidazolium tetrafluoroborate or 1-ethyl-3-methylimidazolium tetrafluoroborate (1) + cyclopentanone or cyclohexanone (2) binary

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ionic liquid mixtures have been reported over entire composition range at (293.15, 298.15, 303.15 and 308.15) K. The topology of the constituent molecules (Graph theory) has been successfully utilized to compute excess heat capacities C_P^E of the studied mixtures [11–14]. In the present paper, we extend our study to ternary mixtures and report excess heat capacities, $(C_P^E)_{123}$, of ternary 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-butyl-3-methylimidazolium tetrafluoroborate or 1-ethyl-3-methylimidazolium tetrafluoroborate (2) + cyclopentanone or cyclohexanone (3) mixtures over the temperature range (293.15–308.15) K having interval of 5 K. The $(C_P^E)_{123}$ data of the said mixtures are not available in the literature. Further, it would be of interest to show how the Graph theory (which in turn deals with the topology of the constituent molecules) describes the $(C_P^E)_{123}$ values of present ternary mixtures. These considerations prompted use to measure molar heat capacities $(C_P)_{123}$ data of 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-butyl-3-methylimidazolium tetrafluoroborate or 1-ethyl-3-methylimidazolium tetrafluoroborate (2) + cyclopentanone or cyclohexanone (3) mixtures at (293.15, 298.15, 303.15 and 308.15) K.

Experimental

Materials

Ionic liquids (ILs) used in this work: 1-butyl-2,3-dimethylimidazolium tetrafluoroborate [Bmmim][BF₄]; (mass fraction: ≥ 0.998), 1-butyl-3-methylimidazolium tetrafluoroborate [Bmim][BF₄]; (mass fraction: ≥ 0.993) and 1-ethyl-3-methylimidazolium tetrafluoroborate [Emim][BF₄]; (mass fraction: ≥ 0.990) obtained from Fluka were used for measurements without further purification. The water content in present ILs was estimated periodically by Karl Fischer Titration and was found to be less than (180–220) ppm [15]. Cyclopentanone (Fluka, mass fraction: ≥ 0.995) and cyclohexanone (Fluka, mass fraction: ≥ 0.990) were purified by standard methods [16]. The purification procedure and analysis methods of all chemicals used in this study along with their suppliers, CAS number and stated purities are given in Table 1.

The densities, ρ , and speeds of sound, u , values were measured to check the purity of the purified liquids at the studied temperatures using an vibrating tube densitometer (Anton Paar DSA 5000) with an estimated accuracy of $\pm 0.5 \text{ kg m}^{-3}$ and 0.5 m s^{-1} , respectively, in the manner as described elsewhere [17, 18]. Such ρ and u values along with their literature values [14, 19–37] are reported in Table 2. It has been observed that measured ρ and u values are in agreement with the literature values.

Apparatus and procedure

Molar heat capacities of pure liquids and the investigated ternary mixtures were measured by a high-sensitivity micro-differential scanning calorimeter Micro-DSC (Model— μ DSC 7 Evo), from M/S SETARAM, France, in the manner as described elsewhere [38]. The calorimeter is based on the Tian–Calvet principle, which determines the change of heat flow from/to the liquid sample upon temperature scanning of $0.4 \text{ }^\circ\text{C min}^{-1}$ and uses a double-stage temperature control with Peltier coolers that works between -45 and $120 \text{ }^\circ\text{C}$. The calibration of calorimeter was done by Joule effect method and checked by measuring heat of fusion of naphthalene which was found to be 148.51 J g^{-1} which in turn was comparable to literature value 148.7 J g^{-1} [39]. The instrument is comprised of two differentially assembled reference and experimental batch cells lodged in a calorimetric block immersed in an inert atmosphere of nitrogen gas (constant sweeping of nitrogen gas at 0.8 bar pressure). Pure liquid or a mixture of known composition was taken in the experimental batch cell with the help of micropipette. Ternary mixtures were prepared by weighing the components using a digital electronic balance (Mettler AX-205) with an uncertainty of $\pm 1 \times 10^{-5} \text{ g}$ for all measurements and kept in air-tight glass bottles to minimize the absorption of atmospheric moisture. The estimated uncertainty in the mole fraction was found to be $\pm 1 \times 10^{-4}$. The equipment was scanned for temperature cycle $15 \text{ }^\circ\text{C}$ (initial temperature) and $45 \text{ }^\circ\text{C}$ (final temperature) at the scanning (heating or cooling) rate $0.4 \text{ }^\circ\text{C min}^{-1}$. The stability in the calorimetric signal was

Table 1 Details of chemical source, CAS number, purification method, final purities and analysis methods

Chemical name	Source	CAS number	Purification method	Final purity (mass fraction)	Analysis method
1-butyl-2,3-dimethyl imidazolium tetrafluoroborate	Fluka	402846-78-0	Used as received	≥ 0.998	–
1-butyl-3-methyl imidazolium tetrafluoroborate	Fluka	174501-65-6	Used as such	≥ 0.993	–
1-ethyl-3-methyl imidazolium tetrafluoroborate	Fluka	143314-16-3	Used as such	≥ 0.990	–
Cyclopentanone	Fluka	120-92-3	Fractional distillation	≥ 0.995	GC
Cyclohexanone	Fluka	108-94-1	Fractional distillation	≥ 0.990	GC

GC gas chromatography

Table 2 Comparison of experimental densities, ρ , speeds of sound, u , and molar heat capacities, C_p , values of pure components with literature values at $T = (293.15\text{--}308.15)$ K

Components	T/K	$\rho/\text{kg m}^{-3}$		$u/\text{m s}^{-1}$		$C_p/\text{J K}^{-1} \text{mol}^{-1}$	
		Expt.	Lit.	Expt.	Lit.	Expt.	Lit.
[Bmmim][BF ₄]	293.15	1193.5	1196.716 ^a	1659.7	1654.88 ^a	413.03	–
	298.15	1191.8	1191.2 ^b	1645.7	1641.44 ^a	416.01	–
			1193.338 ^a				
			1193.19 ^c				
	303.15	1189.7	1189.80 ^c	1632.5	1628.74 ^a	418.84	–
308.15	1187.9	1186.516 ^a	1619.8	1616.88 ^a	421.70	–	
[Bmim][BF ₄]	293.15	1203.1	1204.6 ^d	1578.1	1578.0 ^f	362.35	362.31 ^u
			1204.16 ^e				362.5 ^f
			1202.952 ^f				
	298.15	1198.9	1198.78 ^g	1565.5	1565.1 ^f	365.12	364.8 ^f
			1199.387 ^f				366.28 ^g
							1566 ^h
	303.15	1195.3	1195.18 ^g	1554.1	1554 ^f	367.48	367.37 ^u
			1196.98 ^e				367.2 ^f
			1195.818 ^f				
	308.15	1191.7	1192.266 ^f	1542.3	1542 ^f	369.88	369.94 ^u
1191.60 ^g			369.5 ^f				
[Emim][BF ₄]	293.15	1283.9	1284 ⁱ	1631.1	1631.1 ^m	303.20	303.23 ^v
	298.15	1279.9	1280 ⁱ	1619.2	1622.89 ^k	304.53	304.87 ^v
			1280.07 ^j				1629 ^l
	303.15	1276.3	1276 ⁱ	1607.4	1608.1 ^m	306.29	306.58 ^v
	308.15	1272.1	1272 ⁱ	1596.2	1599.47 ^k	308.03	308.36 ^v
1272.48 ^j			1606 ^l				
Cyclopentanone	293.15	949.3	949.34 ^m	1414.6	1414.3 ^m	152.95	152.99 ^m
	298.15	944.5	944.52 ^m	1393.6	1393.2 ^m	154.45	154.69 ^m
			944.35 ⁿ				154.5 ^w
			945.3 ^o				
	303.15	939.7	939.68 ^m	1372.6	1372.5 ^m	155.61	155.74 ^m
	308.15	934.8	934.84 ^m	1352.2	1352.6 ^m	156.76	156.81 ^m
			934.69 ⁿ				
Cyclohexanone	293.15	947.4	947.39 ^m	1431.2	1430.5 ^q	176.17	176.19 ^m
	298.15	942.9	947.80 ^f	1414.5	1408.0 ^p	178.27	178.37 ^m
			942.90 ^m				177.97 ^x
			942.76 ^s				
	303.15	938.1	938.05 ^m	1395.1	1395.6 ^m	180.38	180.46 ^m
			940.3 ^t				
308.15	933.2	933.18 ^m	1375.1	1375.8 ^m	182.46	182.39 ^m	
		933.8 ^s					

Standard uncertainties, u , are $u(T)$ (DSA) = ± 0.01 K; $u(\rho)$ = ± 0.5 kg m⁻³; $u(u)$ = ± 0.5 m s⁻¹; $u(C_p)$ = $\pm 0.8\%$; $u(T)$ (DSC) = ± 0.02 K
^a Ref. [19], ^b Ref. [20], ^c Ref. [21], ^d Ref. [22], ^e Ref. [23], ^f Ref. [24], ^g Ref. [25], ^h Ref. [26], ⁱ Ref. [27], ^j Ref. [28], ^k Ref. [29], ^l Ref. [30],
^m Ref. [14], ⁿ Ref. [31], ^o Ref. [32], ^p Ref. [33], ^q Ref. [34], ^r Ref. [35], ^s Ref. [36], ^t Ref. [37], ^u Ref. [40], ^v Ref. [41], ^w Ref. [42], ^x Ref. [43]

produced by scanning (900 s) an isothermal level at the initial and final temperature. The temperature cycle and scanning rate of isothermal level was maintained by

software. After scanning, a graph between heat flow and calorimeter temperature along with C_p values was displayed. The C_p values of the purified liquids are

summarized in Table 2 and compared with their literature values [40–43]. The standard uncertainties of the reported C_P values and temperature are estimated to be $\pm 0.8\%$ and ± 0.02 K, respectively.

Results

The molar heat capacities $(C_P)_{123}$ of [Bmmim][BF₄] (1) + [Bmim][BF₄] or [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) ternary mixtures were measured over entire mole fraction of (1) and (2) components in temperature range of (293.15–308.15) K with 5-K interval and are listed in Table 3. The excess heat capacities, $(C_P^E)_{123}$, the difference between the molar heat capacities of the mixture and the summation of the pure components contribution were calculated for the present (1 + 2 + 3) mixtures using expression cited in the work of Lide and Kehiaian [44]:

$$(C_P^E)_{123} = (C_P)_{123} - \sum_{i=1}^3 x_i (C_P)_i \quad (1)$$

where $(C_P)_{123}$, $(C_P)_i$ ($i = 1$ or 2 or 3), x_i ($i = 1$ or 2 or 3) denote molar heat capacities of the ternary mixtures, molar heat capacities and mole fraction of pure component ($i = 1$ or 2 or 3), respectively. The obtained $(C_P^E)_{123}$ values for the investigated mixtures are recorded in Table 3.

The experimental $(C_P^E)_{123}$ data at the studied temperatures were fitted to Redlich–Kister equation [45]:

$$(C_P^E)_{123} = x_1 x_2 \left[\sum_{n=0}^2 (C_P)_{12}^{(n)} (x_1 - x_2)^n \right] + x_2 x_3 \left[\sum_{n=0}^2 (C_P)_{23}^{(n)} (x_2 - x_3)^n \right] + x_1 x_3 \left[\sum_{n=0}^2 (C_P)_{13}^{(n)} (x_1 - x_3)^n \right] + x_1 x_2 x_3 \left[\sum_{n=0}^2 (C_P)_{123}^{(n)} (x_2 - x_3)^n x_1^n \right] \quad (2)$$

where x_1 , x_2 and x_3 are the mole fractions of (1), (2) and (3) components. The $(C_P)_{12}^{(n)}$, $(C_P)_{23}^{(n)}$, $(C_P)_{13}^{(n)}$, ($n = 0-2$), are parameters of sub-binary mixtures (1 + 2), (2 + 3), (1 + 3) of (1 + 2 + 3) mixture and were taken from the literature [11–14]. The $(C_P)_{123}^{(n)}$ ($n = 0-2$) are characteristic parameters of (1 + 2 + 3) mixture and were obtained by fitting the measured $(C_P^E)_{123}$ data to Eq. (2) by least-squares method. The quality of the fit was assessed via the standard deviation, $(C_P^E)_{123}$, expressed as:

Table 3 Comparison of experimental, excess heat capacities $(C_P^E)_{123}$ data for the various (1 + 2 + 3) ternary mixtures with values predicted from the Graph and Flory theories at $T = (293.15-308.15)$ K

x_1	x_2	$(C_P)_{123}/J K^{-1} mol^{-1}$	$(C_P^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
[Bmmim][BF ₄] (1) + [Bmim][BF ₄] (2) + cyclopentanone (3)					
$T/K = 293.15$					
0.0922	0.7616	353.23	16.82	18.48	-0.41
0.1043	0.7529	350.60	12.87	12.87	-0.56
0.1481	0.7191	338.15	-3.90	-4.68	-1.06
0.1705	0.7018	332.87	-11.38	-12.34	-1.29
0.2163	0.6664	325.51	-23.24	-25.35	-1.75
0.2368	0.6403	323.55	-25.07	-27.31	-1.77
0.2772	0.5889	321.24	-27.12	-29.53	-1.76
0.2971	0.5636	320.70	-27.53	-29.86	-1.73
0.3169	0.5385	320.29	-27.84	-29.73	-1.70
0.3364	0.5136	319.62	-28.37	-29.12	-1.65
0.3601	0.4949	320.11	-30.13	-30.13	-1.78
0.3841	0.4759	321.40	-31.10	-30.52	-1.89
0.4084	0.4566	323.22	-31.56	-30.32	-1.99
0.4332	0.4370	325.76	-31.37	-29.59	-2.09
0.4583	0.4172	328.99	-30.51	-28.35	-2.17
0.4838	0.3970	332.94	-28.97	-26.62	-2.23
0.5064	0.3742	337.06	-25.95	-23.63	-2.17
0.5198	0.3566	340.33	-22.48	-20.83	-2.05
0.5328	0.3395	343.64	-18.97	-18.09	-1.93
0.5453	0.3230	346.97	-15.44	-15.44	-1.80
0.5575	0.3070	350.22	-12.01	-12.87	-1.67
0.5693	0.2915	353.42	-8.63	-10.39	-1.54
0.5807	0.2765	356.44	-5.43	-6.01	-1.41
0.6049	0.2570	361.07	-3.01	-4.18	-1.38
0.6228	0.2454	364.16	-2.15	-3.59	-1.40
0.6405	0.2338	367.19	-1.30	-2.00	-1.42
0.6581	0.2224	370.21	-0.47	-0.46	-1.43
0.6680	0.2087	372.00	1.62	1.62	-1.27
0.6846	0.1870	374.35	4.20	4.72	-1.03
0.7011	0.1655	376.79	6.84	7.56	-0.78
0.7175	0.1442	378.82	9.07	10.12	-0.53
0.7709	0.1050	387.17	11.74	13.06	-0.32
$T/K = 298.15$					
0.0922	0.7616	357.42	18.41	20.23	0.01
0.1043	0.7529	354.94	14.60	14.60	-0.11
0.1481	0.7191	342.45	-2.23	-2.99	-0.52
0.1705	0.7018	337.85	-9.04	-10.64	-0.71
0.2163	0.6664	329.46	-21.95	-23.64	-1.09
0.2368	0.6403	327.90	-23.38	-25.58	-1.07
0.2772	0.5889	325.85	-25.17	-27.80	-1.00
0.2971	0.5636	324.66	-26.24	-28.14	-0.96
0.3169	0.5385	324.48	-26.31	-28.04	-0.91
0.3364	0.5136	324.03	-26.61	-27.48	-0.84

Table 3 continued

x_1	x_2	$(C_p)_{123}/J$ $K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.3601	0.4949	324.41	-28.49	-28.49	-0.95
0.3841	0.4759	325.72	-29.45	-28.88	-1.05
0.4084	0.4566	327.36	-30.10	-28.69	-1.14
0.4332	0.4370	329.88	-29.94	-27.97	-1.23
0.4583	0.4172	333.08	-29.13	-26.74	-1.30
0.4838	0.3970	337.12	-27.51	-25.03	-1.36
0.5064	0.3742	341.18	-24.56	-22.10	-1.32
0.5198	0.3566	344.28	-21.26	-19.41	-1.20
0.5328	0.3395	347.63	-17.70	-16.78	-1.09
0.5453	0.3230	350.88	-14.24	-14.24	-0.97
0.5575	0.3070	354.03	-10.91	-11.80	-0.86
0.5693	0.2915	357.14	-7.63	-9.45	-0.74
0.5807	0.2765	360.02	-4.57	-5.20	-0.63
0.6049	0.2570	364.54	-2.27	-3.48	-0.62
0.6228	0.2454	367.57	-1.47	-2.92	-0.66
0.6405	0.2338	370.56	-0.67	-1.36	-0.69
0.6581	0.2224	373.50	0.06	0.14	-0.72
0.6680	0.2087	375.20	2.06	2.06	-0.59
0.6846	0.1870	377.38	4.47	4.88	-0.38
0.7011	0.1655	379.63	6.93	7.42	-0.17
0.7175	0.1442	381.99	9.49	9.66	0.04
0.7709	0.1050	390.28	12.07	12.23	0.15
$T/K = 303.15$					
0.0922	0.7616	361.53	20.29	22.08	0.40
0.1043	0.7529	358.98	16.40	16.40	0.29
0.1481	0.7191	345.80	-1.15	-1.32	-0.05
0.1705	0.7018	341.30	-7.88	-9.02	-0.22
0.2163	0.6664	333.04	-20.70	-22.06	-0.55
0.2368	0.6403	331.65	-21.95	-23.99	-0.51
0.2772	0.5889	329.34	-24.01	-26.21	-0.42
0.2971	0.5636	328.37	-24.85	-26.57	-0.36
0.3169	0.5385	328.03	-25.09	-26.49	-0.30
0.3364	0.5136	327.67	-25.31	-25.97	-0.24
0.3601	0.4949	328.27	-26.98	-26.98	-0.34
0.3841	0.4759	329.62	-27.93	-27.38	-0.43
0.4084	0.4566	331.29	-28.56	-27.19	-0.52
0.4332	0.4370	333.82	-28.41	-26.46	-0.60
0.4583	0.4172	337.15	-27.49	-25.23	-0.67
0.4838	0.3970	341.00	-26.08	-23.50	-0.74
0.5064	0.3742	345.15	-23.04	-20.63	-0.70
0.5198	0.3566	348.08	-19.91	-18.02	-0.60
0.5328	0.3395	351.35	-16.44	-15.48	-0.50
0.5453	0.3230	354.53	-13.05	-13.05	-0.39
0.5575	0.3070	357.62	-9.79	-10.71	-0.29
0.5693	0.2915	360.62	-6.61	-8.47	-0.19
0.5807	0.2765	363.40	-3.65	-4.34	-0.09
0.6049	0.2570	367.83	-1.46	-1.70	-0.10

Table 3 continued

x_1	x_2	$(C_p)_{123}/J$ $K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.6228	0.2454	370.82	-0.72	-1.15	-0.15
0.6405	0.2338	373.78	0.03	0.62	-0.20
0.6581	0.2224	376.68	0.71	0.87	-0.25
0.6680	0.2087	378.29	2.62	2.62	-0.13
0.6846	0.1870	380.33	4.89	5.18	0.04
0.7011	0.1655	382.46	7.23	7.45	0.22
0.7175	0.1442	384.61	9.58	9.39	0.39
0.7709	0.1050	393.24	12.46	11.58	0.42
$T/K = 308.15$					
0.0922	0.7616	365.07	21.57	23.37	0.36
0.1043	0.7529	362.57	17.72	17.72	0.26
0.1481	0.7191	349.41	0.16	0.11	-0.06
0.1705	0.7018	344.39	-7.11	-7.53	-0.22
0.2163	0.6664	336.60	-19.49	-20.45	-0.53
0.2368	0.6403	335.10	-20.86	-22.34	-0.48
0.2772	0.5889	332.89	-22.82	-24.52	-0.38
0.2971	0.5636	332.47	-23.12	-24.89	-0.32
0.3169	0.5385	332.06	-23.42	-24.83	-0.25
0.3364	0.5136	331.67	-23.68	-24.33	-0.18
0.3601	0.4949	332.32	-25.32	-25.32	-0.27
0.3841	0.4759	333.70	-26.25	-25.69	-0.36
0.4084	0.4566	335.55	-26.72	-25.48	-0.44
0.4332	0.4370	337.94	-26.72	-24.74	-0.52
0.4583	0.4172	341.24	-25.86	-23.50	-0.59
0.4838	0.3970	344.92	-24.63	-21.77	-0.66
0.5064	0.3742	349.16	-21.51	-18.96	-0.62
0.5198	0.3566	352.06	-18.42	-16.45	-0.51
0.5328	0.3395	355.19	-15.09	-14.02	-0.41
0.5453	0.3230	358.37	-11.69	-11.69	-0.31
0.5575	0.3070	361.42	-8.48	-9.47	-0.21
0.5693	0.2915	364.28	-5.44	-6.35	-0.11
0.5807	0.2765	366.95	-2.58	-3.34	-0.01
0.6049	0.2570	371.28	-0.51	-0.59	-0.02
0.6228	0.2454	374.23	0.17	0.27	-0.08
0.6405	0.2338	377.14	0.86	0.64	-0.12
0.6581	0.2224	379.99	1.47	1.69	-0.17
0.6680	0.2087	381.51	3.29	3.29	-0.06
0.6846	0.1870	383.36	5.37	5.60	0.11
0.7011	0.1655	385.34	7.56	7.59	0.28
0.7175	0.1442	387.40	9.81	9.25	0.45
0.7709	0.1050	395.97	12.59	11.09	0.46
[Bmmim][BF ₄] (1) + [Bmim][BF ₄] (2) + cyclohexanone (3)					
$T/K = 293.15$					
0.0846	0.7861	373.31	30.75	31.76	-0.01
0.1064	0.7686	363.32	18.85	19.97	-0.26
0.1286	0.7509	355.30	8.87	8.87	-0.51
0.1510	0.7330	347.10	-1.30	-1.34	-0.76

Table 3 continued

x_1	x_2	$(C_p)_{123}/J$ $K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.1737	0.7148	340.84	-9.55	-10.68	-1.00
0.2200	0.6777	331.25	-23.20	-25.82	-1.47
0.2411	0.6517	329.72	-24.89	-26.09	-1.52
0.2826	0.6004	328.73	-26.16	-28.53	-1.57
0.3032	0.5750	328.25	-26.79	-27.88	-1.58
0.3236	0.5498	328.49	-26.68	-26.68	-1.58
0.3677	0.5054	329.02	-28.34	-27.12	-1.69
0.4165	0.4656	331.32	-30.19	-29.30	-1.92
0.4413	0.4453	333.94	-29.66	-29.41	-2.01
0.4666	0.4247	337.42	-28.34	-28.96	-2.09
0.4921	0.4039	341.41	-26.52	-27.96	-2.16
0.5152	0.3807	345.51	-23.57	-24.62	-2.12
0.5292	0.3630	348.26	-20.84	-20.84	-2.01
0.5427	0.3458	351.33	-17.76	-17.15	-1.90
0.5558	0.3292	354.59	-14.51	-13.63	-1.79
0.5685	0.3131	357.81	-11.31	-10.27	-1.68
0.5808	0.2974	360.95	-8.16	-7.03	-1.57
0.5928	0.2822	364.03	-5.09	-3.99	-1.45
0.6171	0.2622	368.88	-2.27	-1.77	-1.42
0.6347	0.2501	372.07	-0.99	-0.93	-1.43
0.6522	0.2381	375.20	0.22	0.24	-1.44
0.6695	0.2263	378.23	1.35	1.08	-1.44
0.6800	0.2124	380.24	3.46	3.46	-1.30
0.6974	0.1905	383.03	6.20	7.11	-1.07
0.7148	0.1687	385.79	8.90	10.22	-0.84
0.7320	0.1471	389.34	12.40	12.70	-0.61
0.7563	0.1268	394.28	15.37	13.59	-0.47
0.7848	0.1069	397.93	15.97	13.53	-0.38
$T/K = 298.15$					
0.0846	0.7861	376.36	31.09	31.36	0.54
0.1064	0.7686	366.32	19.14	19.94	0.34
0.1286	0.7509	358.35	9.20	9.20	0.13
0.1510	0.7330	350.48	-0.65	-0.67	-0.08
0.1737	0.7148	343.87	-9.26	-9.70	-0.28
0.2200	0.6777	335.46	-21.74	-23.30	-0.67
0.2411	0.6517	334.75	-22.61	-24.52	-0.69
0.2826	0.6004	333.72	-23.92	-24.93	-0.68
0.3032	0.5750	333.23	-24.56	-26.30	-0.67
0.3236	0.5498	332.79	-25.15	-25.15	-0.64
0.3677	0.5054	333.31	-26.81	-25.59	-0.73
0.4165	0.4656	335.63	-28.66	-27.72	-0.94
0.4413	0.4453	338.21	-28.18	-27.83	-1.03
0.4666	0.4247	341.61	-26.94	-27.41	-1.11
0.4921	0.4039	345.41	-25.32	-26.45	-1.18
0.5152	0.3807	349.51	-22.38	-23.25	-1.15
0.5292	0.3630	352.28	-19.63	-19.63	-1.05
0.5427	0.3458	355.23	-16.67	-16.10	-0.96

Table 3 continued

x_1	x_2	$(C_p)_{123}/J$ $K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.5558	0.3292	358.29	-13.62	-12.74	-0.86
0.5685	0.3131	361.39	-10.54	-9.53	-0.76
0.5808	0.2974	364.41	-7.51	-6.44	-0.66
0.5928	0.2822	367.39	-4.54	-3.55	-0.56
0.6171	0.2622	372.07	-1.90	-1.44	-0.56
0.6347	0.2501	375.20	-0.70	-0.64	-0.59
0.6522	0.2381	378.25	0.44	0.39	-0.62
0.6695	0.2263	381.21	1.48	1.02	-0.65
0.6800	0.2124	383.13	3.51	3.51	-0.53
0.6974	0.1905	385.80	6.14	6.95	-0.34
0.7148	0.1687	388.74	9.01	9.85	-0.15
0.7320	0.1471	391.92	12.14	12.14	0.04
0.7563	0.1268	396.76	14.99	12.92	0.12
0.7848	0.1069	400.19	15.37	12.80	0.15
$T/K = 303.15$					
0.0846	0.7861	380.47	32.84	31.00	1.04
0.1064	0.7686	370.10	20.54	20.03	0.86
0.1286	0.7509	361.26	9.72	9.72	0.67
0.1510	0.7330	353.76	0.23	0.25	0.49
0.1737	0.7148	346.67	-8.87	-8.40	0.31
0.2200	0.6777	339.31	-20.33	-21.32	-0.04
0.2411	0.6517	338.77	-21.04	-22.44	-0.03
0.2826	0.6004	338.09	-22.01	-24.77	0.01
0.3032	0.5750	337.99	-22.27	-24.15	0.04
0.3236	0.5498	337.39	-23.02	-23.02	0.08
0.3677	0.5054	338.27	-24.35	-23.42	0.01
0.4165	0.4656	340.63	-26.18	-25.40	-0.20
0.4413	0.4453	343.32	-25.61	-25.48	-0.29
0.4666	0.4247	346.42	-24.69	-25.06	-0.38
0.4921	0.4039	350.36	-22.94	-24.11	-0.46
0.5152	0.3807	354.11	-20.36	-21.05	-0.44
0.5292	0.3630	356.87	-17.62	-17.62	-0.35
0.5427	0.3458	359.62	-14.87	-14.28	-0.27
0.5558	0.3292	362.63	-11.88	-11.10	-0.18
0.5685	0.3131	365.53	-9.00	-8.07	-0.10
0.5808	0.2974	368.48	-6.04	-5.17	-0.01
0.5928	0.2822	371.26	-3.28	-2.46	0.07
0.6171	0.2622	375.78	-0.81	-0.78	0.05
0.6347	0.2501	378.80	0.27	0.27	0.02
0.6522	0.2381	381.75	1.30	1.06	-0.05
0.6695	0.2263	384.62	2.25	1.84	-0.09
0.6800	0.2124	386.42	4.15	4.15	0.01
0.6974	0.1905	388.89	6.56	7.28	0.16
0.7148	0.1687	391.58	9.19	9.89	0.31
0.7320	0.1471	394.40	11.94	11.90	0.47
0.7563	0.1268	398.99	14.54	12.51	0.51
0.7848	0.1069	402.85	15.33	12.29	0.49

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
$T/K = 308.15$					
0.0846	0.7861	383.50	33.47	30.69	1.12
0.1064	0.7686	373.54	21.57	20.14	0.94
0.1286	0.7509	364.18	10.22	10.22	0.77
0.1510	0.7330	357.03	1.07	1.12	0.59
0.1737	0.7148	350.44	-7.54	-7.20	0.42
0.2200	0.6777	344.06	-18.05	-20.54	0.09
0.2411	0.6517	343.26	-19.02	-21.59	0.11
0.2826	0.6004	342.48	-20.12	-22.84	0.16
0.3032	0.5750	342.05	-20.71	-22.22	0.20
0.3236	0.5498	341.81	-21.12	-21.12	0.24
0.3677	0.5054	343.17	-21.98	-21.48	0.18
0.4165	0.4656	345.43	-23.94	-23.42	-0.02
0.4413	0.4453	347.96	-23.54	-23.50	-0.11
0.4666	0.4247	351.00	-22.68	-23.11	-0.20
0.4921	0.4039	354.86	-21.03	-22.22	-0.28
0.5152	0.3807	358.51	-18.56	-19.29	-0.26
0.5292	0.3630	361.10	-16.00	-16.00	-0.17
0.5427	0.3458	363.91	-13.19	-12.80	-0.09
0.5558	0.3292	366.67	-10.46	-9.76	-0.01
0.5685	0.3131	369.55	-7.59	-6.87	0.08
0.5808	0.2974	372.31	-4.84	-4.10	0.16
0.5928	0.2822	375.00	-2.18	-1.51	0.25
0.6171	0.2622	379.36	0.12	0.15	0.22
0.6347	0.2501	382.29	1.11	1.05	0.17
0.6522	0.2381	385.17	2.05	1.77	0.12
0.6695	0.2263	387.95	2.91	2.50	0.07
0.6800	0.2124	389.63	4.68	4.68	0.16
0.6974	0.1905	391.96	6.95	7.64	0.31
0.7148	0.1687	394.67	9.58	10.08	0.46
0.7320	0.1471	397.51	12.36	11.93	0.61
0.7563	0.1268	401.24	14.08	12.44	0.64
0.7848	0.1069	405.51	15.26	12.15	0.61
[Bmmim][BF ₄] (1) + [Emim][BF ₄] (2) + cyclopentanone (3)					
$T/K = 293.15$					
0.0814	0.7865	300.34	8.05	8.27	1.37
0.1108	0.7626	310.41	14.06	13.65	1.21
0.1305	0.7471	316.47	17.33	16.94	1.10
0.1506	0.7313	323.45	21.46	20.04	0.99
0.1710	0.7151	327.77	22.91	22.91	0.88
0.1908	0.6949	331.62	24.63	25.19	0.83
0.2107	0.6745	335.29	26.20	27.20	0.78
0.2308	0.6539	338.65	27.42	28.96	0.73
0.2511	0.6332	341.98	28.58	30.47	0.69
0.2700	0.6089	344.98	30.33	31.33	0.71
0.3078	0.5605	350.71	33.49	32.38	0.75
0.3265	0.5364	353.19	34.73	32.54	0.78

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.3491	0.5181	355.68	34.09	33.08	0.70
0.3721	0.4994	358.12	33.36	33.36	0.62
0.3956	0.4803	360.53	32.53	33.36	0.54
0.4195	0.4608	362.56	31.27	33.10	0.46
0.4661	0.4183	366.01	28.99	31.50	0.39
0.4885	0.3954	367.31	27.90	30.20	0.39
0.5048	0.3800	368.25	26.92	29.23	0.38
0.5179	0.3628	368.96	26.80	27.98	0.43
0.5306	0.3460	369.63	26.70	26.70	0.49
0.5430	0.3297	370.01	26.30	25.39	0.54
0.5551	0.3138	370.71	26.24	24.06	0.60
0.5669	0.2983	371.34	26.13	22.72	0.66
0.5914	0.2780	372.24	23.71	20.82	0.63
0.6092	0.2658	372.79	21.46	19.60	0.58
0.6270	0.2538	373.15	19.00	18.36	0.52
0.6446	0.2417	373.40	16.49	17.08	0.48
0.6552	0.2273	373.14	15.64	15.64	0.55
0.6730	0.2043	372.83	14.15	13.30	0.66
0.7085	0.1585	371.83	10.80	8.57	0.89
0.7340	0.1371	370.63	6.18	6.32	0.91
$T/K = 298.15$					
0.0814	0.7865	302.40	8.62	7.22	1.55
0.1108	0.7626	312.74	14.86	13.46	1.44
0.1305	0.7471	319.23	18.52	17.28	1.35
0.1506	0.7313	326.12	22.53	20.85	1.27
0.1710	0.7151	330.64	24.14	24.14	1.18
0.1908	0.6949	334.54	25.90	26.73	1.15
0.2107	0.6745	338.54	27.75	29.00	1.12
0.2308	0.6539	342.08	29.12	30.98	1.10
0.2511	0.6332	345.75	30.60	32.67	1.07
0.2700	0.6089	348.74	32.29	33.63	1.11
0.3078	0.5605	354.51	35.43	34.79	1.19
0.3265	0.5364	357.24	36.89	34.99	1.23
0.3491	0.5181	360.05	36.54	35.59	1.16
0.3721	0.4994	362.61	35.88	35.88	1.10
0.3956	0.4803	364.93	34.93	35.86	1.03
0.4195	0.4608	366.86	33.53	35.53	0.96
0.4661	0.4183	370.52	31.37	33.69	0.90
0.4885	0.3954	371.76	30.19	32.26	0.90
0.5048	0.3800	372.67	29.15	31.17	0.89
0.5179	0.3628	373.26	28.90	29.86	0.94
0.5306	0.3460	373.68	28.52	28.52	1.00
0.5430	0.3297	374.09	28.13	27.16	1.06
0.5551	0.3138	374.41	27.67	25.79	1.12
0.5669	0.2983	374.88	27.38	24.41	1.17
0.5914	0.2780	375.74	24.88	22.35	1.14
0.6092	0.2658	376.07	22.39	20.97	1.08

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.6270	0.2538	376.45	19.91	19.57	1.02
0.6446	0.2417	376.80	17.47	18.12	0.96
0.6552	0.2273	376.65	16.71	16.71	1.03
0.6730	0.2043	376.33	15.19	14.44	1.13
0.7085	0.1585	374.93	11.38	10.00	1.35
0.7340	0.1371	373.89	6.88	7.78	1.34
$T/K = 303.15$					
0.0814	0.7865	304.98	9.43	8.59	1.64
0.1108	0.7626	315.27	15.59	14.68	1.52
0.1305	0.7471	321.75	19.22	18.40	1.43
0.1506	0.7313	328.84	23.39	21.88	1.34
0.1710	0.7151	333.46	25.08	25.08	1.25
0.1908	0.6949	337.44	26.89	27.64	1.22
0.2107	0.6745	341.51	28.81	29.90	1.19
0.2308	0.6539	345.13	30.24	31.87	1.16
0.2511	0.6332	348.89	31.77	33.56	1.14
0.2700	0.6089	351.92	33.49	34.57	1.18
0.3078	0.5605	357.75	36.66	35.87	1.26
0.3265	0.5364	360.53	38.15	36.13	1.31
0.3491	0.5181	363.40	37.83	36.73	1.23
0.3721	0.4994	365.82	37.01	37.01	1.16
0.3956	0.4803	368.21	36.10	37.00	1.09
0.4195	0.4608	370.36	34.90	36.67	1.02
0.4661	0.4183	373.90	32.57	34.92	0.95
0.4885	0.3954	375.32	31.55	33.55	0.96
0.5048	0.3800	376.40	30.65	32.51	0.95
0.5179	0.3628	376.97	30.36	31.26	1.01
0.5306	0.3460	377.40	29.98	29.98	1.07
0.5430	0.3297	378.02	29.80	28.69	1.13
0.5551	0.3138	378.58	29.57	27.38	1.19
0.5669	0.2983	378.98	29.20	26.05	1.25
0.5914	0.2780	379.86	26.69	24.01	1.22
0.6092	0.2658	380.35	24.33	22.64	1.16
0.6270	0.2538	380.84	21.94	21.23	1.09
0.6446	0.2417	381.11	19.40	19.78	1.04
0.6552	0.2273	380.73	18.40	18.40	1.11
0.6730	0.2043	380.43	16.88	16.17	1.22
0.7085	0.1585	378.77	12.78	11.76	1.44
0.7340	0.1371	377.74	8.26	9.50	1.44
$T/K = 308.15$					
0.0814	0.7865	306.97	9.67	7.99	1.72
0.1108	0.7626	317.70	16.23	14.92	1.60
0.1305	0.7471	325.23	20.88	19.12	1.51
0.1506	0.7313	331.05	23.77	23.02	1.42
0.1710	0.7151	336.82	26.58	26.58	1.34
0.1908	0.6949	341.02	28.59	29.41	1.31
0.2107	0.6745	345.33	30.71	31.90	1.28

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.2308	0.6539	349.15	32.33	34.07	1.25
0.2511	0.6332	353.12	34.05	35.92	1.23
0.2700	0.6089	356.32	35.91	37.11	1.27
0.3078	0.5605	362.42	39.33	38.71	1.36
0.3265	0.5364	365.08	40.67	39.13	1.41
0.3491	0.5181	368.28	40.66	39.71	1.34
0.3721	0.4994	370.81	39.92	39.92	1.27
0.3956	0.4803	373.29	39.06	39.79	1.20
0.4195	0.4608	375.66	38.05	39.30	1.13
0.4661	0.4183	378.99	35.47	37.26	1.06
0.4885	0.3954	380.33	34.33	35.84	1.07
0.5048	0.3800	381.34	33.35	34.70	1.06
0.5179	0.3628	381.78	32.92	33.60	1.12
0.5306	0.3460	382.16	32.48	32.48	1.18
0.5430	0.3297	382.66	32.16	31.36	1.24
0.5551	0.3138	383.15	31.85	30.23	1.31
0.5669	0.2983	383.58	31.50	29.11	1.37
0.5914	0.2780	384.48	28.98	26.95	1.33
0.6092	0.2658	385.01	26.64	25.36	1.27
0.6270	0.2538	385.53	24.26	23.71	1.20
0.6446	0.2417	385.86	21.76	22.03	1.14
0.6552	0.2273	385.73	21.00	21.00	1.22
0.6730	0.2043	385.33	19.36	19.32	1.33
0.7085	0.1585	383.48	15.03	16.27	1.56
0.7340	0.1371	382.27	10.30	14.32	1.56
[Bmmim][BF ₄] (1) + [Emim][BF ₄] (2) + cyclohexanone (3)					
$T/K = 293.15$					
0.0959	0.7916	309.47	10.03	11.64	1.72
0.1161	0.7751	313.75	11.62	12.91	1.61
0.1576	0.7413	321.69	14.02	14.47	1.36
0.1780	0.7204	324.89	15.05	15.05	1.30
0.1986	0.6994	328.06	16.00	15.59	1.24
0.2194	0.6781	331.00	16.72	16.10	1.18
0.2404	0.6567	333.79	17.26	16.56	1.12
0.2603	0.6320	336.22	18.11	17.22	1.13
0.2801	0.6073	338.67	19.01	17.81	1.14
0.2999	0.5827	341.06	19.84	18.33	1.16
0.3197	0.5581	343.53	20.74	18.77	1.17
0.3429	0.5387	346.02	20.20	18.76	1.07
0.3664	0.5191	348.27	19.38	18.71	0.98
0.3904	0.4990	350.66	18.63	18.63	0.88
0.4149	0.4786	352.79	17.55	18.50	0.79
0.4398	0.4577	355.06	16.57	18.34	0.70
0.4628	0.4343	357.26	16.30	18.24	0.68
0.5030	0.3945	361.00	15.58	17.86	0.65
0.5171	0.3767	362.53	16.03	17.72	0.70
0.5307	0.3594	363.91	16.38	17.53	0.74

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.5441	0.3426	365.29	16.72	17.28	0.79
0.5571	0.3261	366.67	17.12	16.99	0.84
0.5697	0.3101	367.86	17.36	16.66	0.89
0.5948	0.2889	369.70	15.95	15.95	0.84
0.6128	0.2760	370.99	14.61	15.43	0.78
0.6307	0.2632	372.33	13.34	14.90	0.72
0.6599	0.2357	374.48	12.06	13.82	0.73
0.6789	0.2120	375.86	11.96	12.83	0.82
0.6979	0.1883	377.06	11.67	11.67	0.92
0.7169	0.1647	377.95	11.05	10.32	1.01
0.7428	0.1424	379.55	9.35	8.85	1.01
0.7730	0.1203	381.88	7.33	7.29	0.97
$T/K = 298.15$					
0.0959	0.7916	312.02	11.00	12.51	1.96
0.1161	0.7751	316.53	12.79	13.95	1.87
0.1576	0.7413	324.58	15.24	15.81	1.68
0.1780	0.7204	328.05	16.50	16.50	1.64
0.1986	0.6994	331.18	17.39	17.15	1.60
0.2194	0.6781	334.33	18.28	17.75	1.56
0.2404	0.6567	337.24	18.90	18.30	1.53
0.2603	0.6320	339.76	19.81	19.02	1.56
0.2801	0.6073	342.30	20.77	19.66	1.59
0.2999	0.5827	344.89	21.75	20.21	1.62
0.3197	0.5581	347.31	22.57	20.67	1.65
0.3429	0.5387	349.77	21.96	20.69	1.57
0.3664	0.5191	352.21	21.29	20.66	1.48
0.3904	0.4990	354.67	20.58	20.58	1.40
0.4149	0.4786	356.94	19.60	20.44	1.31
0.4398	0.4577	359.05	18.44	20.25	1.23
0.4628	0.4343	361.26	18.13	20.10	1.22
0.5030	0.3945	365.04	17.37	19.62	1.19
0.5171	0.3767	366.44	17.67	19.42	1.24
0.5307	0.3594	367.92	18.10	19.18	1.28
0.5441	0.3426	369.15	18.27	18.87	1.33
0.5571	0.3261	370.47	18.58	18.52	1.38
0.5697	0.3101	371.51	18.65	18.13	1.43
0.5948	0.2889	373.47	17.32	17.32	1.37
0.6128	0.2760	374.67	15.87	16.74	1.30
0.6307	0.2632	376.01	14.57	16.14	1.24
0.6599	0.2357	378.09	13.18	14.93	1.23
0.6789	0.2120	379.39	12.95	13.82	1.31
0.6979	0.1883	380.51	12.55	12.55	1.39
0.7169	0.1647	381.26	11.76	11.08	1.47
0.7428	0.1424	382.92	10.08	9.49	1.45
0.7730	0.1203	385.21	7.97	7.80	1.37
$T/K = 303.15$					
0.0959	0.7916	314.76	11.84	12.19	2.15

Table 3 continued

x_1	x_2	$(C_p)_{123}/J K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.1161	0.7751	319.32	13.66	14.75	2.05
0.1576	0.7413	327.57	16.28	16.82	1.84
0.1780	0.7204	331.14	17.61	17.61	1.79
0.1986	0.6994	334.36	18.56	18.33	1.75
0.2194	0.6781	337.59	19.52	19.01	1.71
0.2404	0.6567	340.49	20.10	19.62	1.67
0.2603	0.6320	343.18	21.15	20.39	1.70
0.2801	0.6073	345.78	22.15	21.07	1.74
0.2999	0.5827	348.43	23.17	21.66	1.77
0.3197	0.5581	350.90	24.02	22.15	1.81
0.3429	0.5387	353.40	23.43	22.19	1.71
0.3664	0.5191	355.89	22.78	22.16	1.62
0.3904	0.4990	358.38	22.08	22.08	1.53
0.4149	0.4786	360.69	21.11	21.93	1.43
0.4398	0.4577	362.82	19.93	21.71	1.34
0.4628	0.4343	365.12	19.70	21.54	1.33
0.5030	0.3945	368.80	18.81	20.99	1.29
0.5171	0.3767	370.26	19.15	20.77	1.34
0.5307	0.3594	371.63	19.45	20.50	1.40
0.5441	0.3426	372.83	19.57	20.17	1.44
0.5571	0.3261	374.12	19.84	19.79	1.50
0.5697	0.3101	375.13	19.86	19.37	1.55
0.5948	0.2889	377.09	18.50	18.50	1.49
0.6128	0.2760	378.27	17.01	17.86	1.41
0.6307	0.2632	379.53	15.61	17.21	1.34
0.6599	0.2357	381.63	14.21	15.91	1.33
0.6789	0.2120	382.87	13.91	14.76	1.41
0.6979	0.1883	383.94	13.43	13.43	1.50
0.7169	0.1647	384.70	12.63	11.92	1.59
0.7428	0.1424	386.19	10.75	10.25	1.56
0.7730	0.1203	388.42	8.57	8.48	1.48
$T/K = 308.15$					
0.0959	0.7916	317.18	12.37	13.15	2.24
0.1161	0.7751	321.84	14.27	15.01	2.14
0.1576	0.7413	330.37	17.12	17.58	1.93
0.1780	0.7204	334.03	18.53	18.53	1.89
0.1986	0.6994	337.36	19.56	19.40	1.85
0.2194	0.6781	340.69	20.59	20.19	1.81
0.2404	0.6567	343.67	21.24	20.89	1.77
0.2603	0.6320	346.55	22.45	21.70	1.81
0.2801	0.6073	349.21	23.48	22.41	1.85
0.2999	0.5827	351.80	24.42	23.01	1.89
0.3197	0.5581	354.18	25.16	23.50	1.93
0.3429	0.5387	357.00	24.86	23.57	1.83
0.3664	0.5191	359.42	24.12	23.55	1.74
0.3904	0.4990	361.97	23.46	23.46	1.64
0.4149	0.4786	364.32	22.50	23.26	1.55

Table 3 continued

x_1	x_2	$(C_p)_{123}/J$ $K^{-1} mol^{-1}$	$(C_p^E)_{123}/J K^{-1} mol^{-1}$		
			Exptl.	Graph	Flory
0.4398	0.4577	366.47	21.32	22.98	1.46
0.4628	0.4343	368.66	20.94	22.73	1.44
0.5030	0.3945	372.30	19.96	21.03	1.41
0.5171	0.3767	373.69	20.22	21.75	1.46
0.5307	0.3594	375.10	20.55	21.42	1.52
0.5441	0.3426	376.33	20.68	21.05	1.57
0.5571	0.3261	377.46	20.77	20.63	1.62
0.5697	0.3101	378.50	20.80	20.17	1.67
0.5948	0.2889	380.23	19.19	19.19	1.61
0.6128	0.2760	381.59	17.87	18.47	1.53
0.6307	0.2632	382.76	16.36	17.73	1.46
0.6599	0.2357	384.80	14.87	15.34	1.44
0.6789	0.2120	386.04	14.53	15.19	1.53
0.6979	0.1883	386.97	13.90	13.90	1.62
0.7169	0.1647	387.62	12.97	12.45	1.71
0.7428	0.1424	389.16	11.11	10.80	1.68
0.7730	0.1203	391.42	8.92	9.02	1.59

Standard uncertainties, u , are $u(C_p)_{123} = \pm 0.8\%$; $u(C_p^E)_{123} = \pm 1.1\%$; $u(T)$ (DSC) = ± 0.02 K

$$\sigma(C_p^E)_{123} = \left\{ \left[\sum (C_p^E)_{123} - (C_p^E)_{123\{calc.Eq.(2)\}} \right]^2 / (m - n) \right\}^{0.5} \quad (3)$$

where m is the number of data points and n is the number of ternary adjustable parameters of Eq. (2), which are presented in Table 4. It was found that Redlich–Kister equation represents satisfactorily the experimental $(C_p^E)_{123}$ for the examined mixtures. The various surfaces generated by $(C_p^E)_{123}$ values of the studied mixtures at 298.15 K are shown in Figs. 1–4.

Discussion

The measured $(C_p)_{123}$ data for [Bmmim][BF₄] (1) + [Bmim][BF₄] or [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures at (293.15, 298.15, 303.15 and 308.15) K are not available in the literature with which the observed data can be compared. The $(C_p^E)_{123}$ data of [Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) are positive over entire composition range of (1) and (2) components of the mixtures. However, the sign as well as magnitude of $(C_p^E)_{123}$ values for [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures are

dictated by the relative proportion of the constituents. The $(C_p^E)_{123}$ data of mixture indicate the variation of mixture entropy with that of ideal system [46]. The $(C_p^E)_{123}$ data of [Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) suggest the contribution to $(C_p^E)_{123}$ due to the formation of 1:2:3 molecular complex (possessing non-random structure) in mixed state far outweighs the contribution due to the destruction of molecular entities of [Bmmim][BF₄] or [Emim][BF₄] or cyclopentanone or cyclohexanone which in turn enhance randomness and increase in entropy of the mixture. Further, $(C_p^E)_{123}$ values of [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclohexanone (3) mixture are higher than those of [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone (3) mixture which in turn indicate strong interactions between the cyclohexanone and [Bmmim][BF₄]: [Bmim][BF₄] molecular entity as compared to cyclopentanone. This may be due to reason that cyclohexanone is more basic in nature and possess chair form [47] and thus can interact strongly and packed efficiently with [Bmmim][BF₄]: [Bmim][BF₄] molecular entity [11].

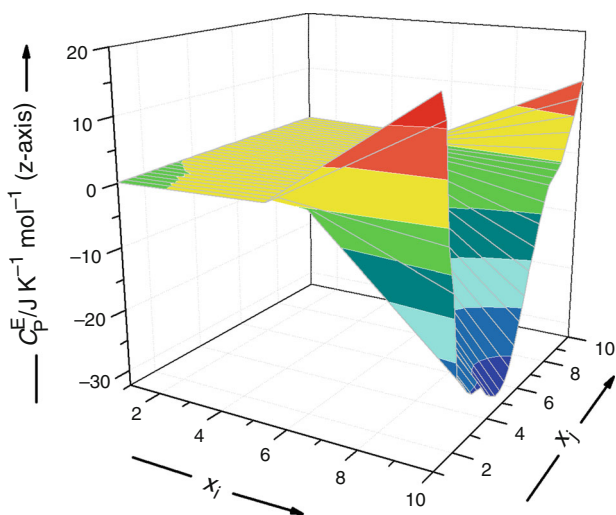
The $(C_p^E)_{123}$ values of [Bmmim][BF₄] (1) + [Bmim][BF₄] or [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures suggest strong interactions between cyclopentanone or cyclohexanone and [Bmmim][BF₄]: [Emim][BF₄] as compared to [Bmmim][BF₄]: [Bmim][BF₄] molecular entity. It may be due to the presence of bulky –CH₃ group in [Bmim][BF₄] which in turn restricts the approach of cyclopentanone or cyclohexanone toward [Bmmim][BF₄]: [Bmim][BF₄] molecular entity. The $\partial(C_p^E)_{123}/\partial T$ for the studied ternary mixtures is positive indicating the rupture of interactions among molecular entities [Bmmim][BF₄] or [Bmim][BF₄] or [Emim][BF₄] or cyclopentanone or cyclohexanone is more difficult in pure state as compared to mixed state [48].

Graph theory

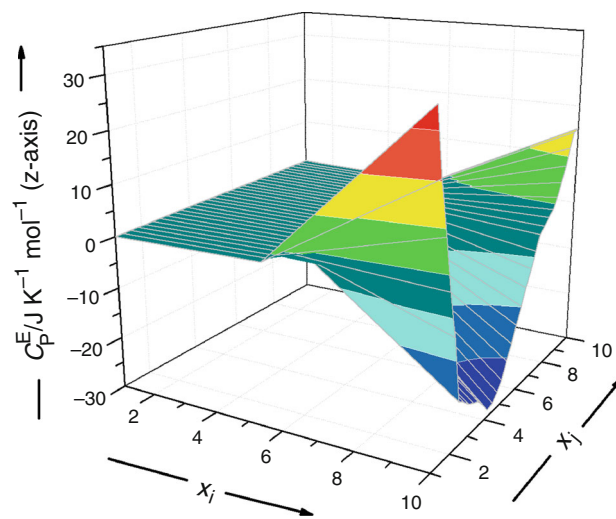
The Moelwyn–Huggins concept [49, 50] of interaction between the surfaces of components of [Bmmim][BF₄] (1) + [Bmim][BF₄] or [Emim][BF₄] (2); [Bmmim][BF₄] or [Bmim][BF₄] (1) + cyclopentanone or cyclohexanone (2) binary mixtures has been successfully utilized (taking into consideration the topology of the components of the mixture) to determine excess molar volumes, V^E , excess isentropic compressibilities, (κ_S^E) , excess heat capacities, C_p^E , and excess molar enthalpies, H^E of (1 + 2) mixtures. The analyses of V^E , (κ_S^E) , C_p^E and H^E data in terms of Moelwyn–Huggins concept (Graph theory), IR and quantum mechanical studies have revealed that ILs: [Bmmim][BF₄], [Bmim][BF₄] and [Emim][BF₄] exist as

Table 4 Ternary adjustable parameters, $(C_p)^{(n)}$ ($n = 0-2$) parameters along with the standard deviations, $\sigma(C_p^E)_{123}$, at $T = (293.15-308.15)$ K

Parameters	T/K			
	293.15	298.15	303.15	308.15
[Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone (3)				
$C_p^{(0)}/J\ K^{-1}\ mol^{-1}$	51.29	57.94	62.06	67.69
$C_p^{(1)}/J\ K^{-1}\ mol^{-1}$	-4957.51	-4201.33	-3524.14	-2804.84
$C_p^{(2)}/J\ K^{-1}\ mol^{-1}$	-76,033.44	-76,466.46	-76,348.92	-76,631.42
$\sigma(C_p^E)_{123}/J\ K^{-1}\ mol^{-1}$	0.05	0.05	0.04	0.04
[Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclohexanone (3)				
$C_p^{(0)}/J\ K^{-1}\ mol^{-1}$	69.88	99.50	144.83	186.65
$C_p^{(1)}/J\ K^{-1}\ mol^{-1}$	-4093.56	-3881.24	-3621.66	-3404.42
$C_p^{(2)}/J\ K^{-1}\ mol^{-1}$	-73,658.90	-71,067.16	-67,477.10	-64,550.59
$\sigma(C_p^E)_{123}/J\ K^{-1}\ mol^{-1}$	0.04	0.04	0.04	0.04
[Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone (3)				
$C_p^{(0)}/J\ K^{-1}\ mol^{-1}$	1101.64	1090.22	1080.66	1069.62
$C_p^{(1)}/J\ K^{-1}\ mol^{-1}$	3283.18	3387.79	3502.49	3880.62
$C_p^{(2)}/J\ K^{-1}\ mol^{-1}$	-9193.28	-6077.61	-5629.29	-3450.75
$\sigma(C_p^E)_{123}/J\ K^{-1}\ mol^{-1}$	0.07	0.07	0.07	0.08
[Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclohexanone (3)				
$C_p^{(0)}/J\ K^{-1}\ mol^{-1}$	1081.34	1099.14	1127.77	1135.38
$C_p^{(1)}/J\ K^{-1}\ mol^{-1}$	1166.69	1030.55	816.01	617.81
$C_p^{(2)}/J\ K^{-1}\ mol^{-1}$	-14,572.93	-12,089.50	-10,528.08	-8337.23
$\sigma(C_p^E)_{123}/J\ K^{-1}\ mol^{-1}$	0.04	0.04	0.05	0.05

**Fig. 1** Surface generated for 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-butyl-3-methylimidazolium tetrafluoroborate (2) + cyclopentanone (3) by excess heat capacities $(C_p^E)_{123}$ data at 298.15 K

monomer (characterized by cohesion forces; H-bonding occurs between hydrogen atom/s of methyl group/s attached to imidazolium ring with fluorine atoms of BF_4

**Fig. 2** Surface generated for 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-butyl-3-methylimidazolium tetrafluoroborate (2) + cyclohexanone (3) by excess heat capacities $(C_p^E)_{123}$ data at 298.15 K

[11]); cyclopentanone, cyclohexanone are characterized by dipole-dipole interactions as well as Debye and London forces and exist as associated molecular entities.

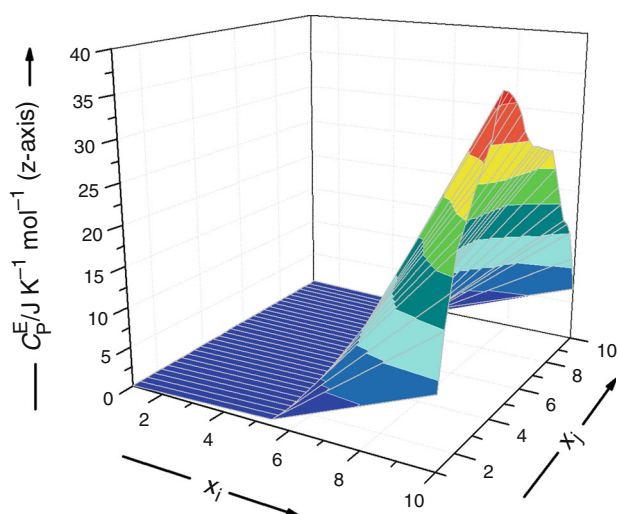


Fig. 3 Surface generated for 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-ethyl-3-methylimidazolium tetrafluoroborate (2) + cyclopentanone (3) by excess heat capacities (C_p^E)₁₂₃ data at 298.15 K

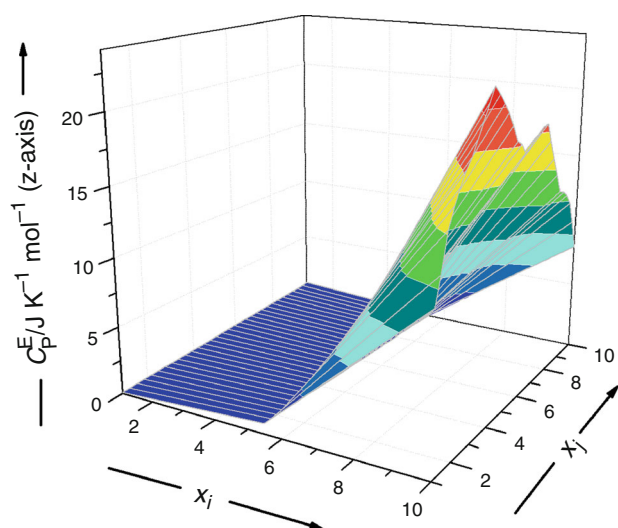


Fig. 4 Surface generated for 1-butyl-2,3-dimethylimidazolium tetrafluoroborate (1) + 1-ethyl-3-methylimidazolium tetrafluoroborate (2) + cyclohexanone (3) by excess heat capacities (C_p^E)₁₂₃ data at 298.15 K

The addition of third component like cyclopentanone or cyclohexanone to molecular entities [Bmmim][BF₄]; [Bmim][BF₄] and [Bmmim][BF₄]; [Emim][BF₄] results in the formation of ternary [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone or cyclohexanone (3) and [Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures. The various processes involved in (1 + 2 + 3) mixtures formation may be assumed to be comprised of the processes: (I) establishment of unlike (a) 1–2, (b) 2–3_n ($n = 2$), (c) 1–3_n contacts; (II) unlike contact formation then leads to rupture of

(a) cohesion forces in [Bmmim][BF₄] or [Bmim][BF₄] or [Emim][BF₄]; and (b) dipole–dipole interactions in cyclopentanone or cyclohexanone which in turn yields their respective monomers; and (III) molecules of 1, 2 and 3 then undergo interactions to form (a) 1:2 (b) 2:3 and (c) 1:3 molecular complexes.

If χ_{12} , χ_{23} , χ_{13} are molar interaction parameters for (I) unlike 1–2; 2–3_n; 1–3_n contacts (leading to enhancement of non-randomness); then change in thermodynamic property, ΔC_p , due to processes I (a)–(c) was expressed by [51–53].

$$(\Delta C_p)_I = \left[\frac{x_1 x_2 ({}^3 \xi_1 / {}^3 \xi_2) \chi_{12}}{x_1 + x_2 ({}^3 \xi_1 / {}^3 \xi_2)} \right] + \left[\frac{x_2 x_3 ({}^3 \xi_2 / {}^3 \xi_3) \chi_{23}}{x_2 + x_3 ({}^3 \xi_2 / {}^3 \xi_3)} \right] + \left[\frac{x_3 x_1 ({}^3 \xi_3 / {}^3 \xi_1) \chi_{13}}{x_3 + x_1 ({}^3 \xi_3 / {}^3 \xi_1)} \right] \quad (4)$$

Further, if χ_{11} , χ_{22} , χ_{33} ; and χ'_{12} , χ''_{12} , χ'''_{12} are molar interaction parameters for rupture of cohesion forces in ILs and dipole–dipole interactions in cyclopentanone and cyclohexanone (increase in randomness) and specific interactions between 1, 2 and 3 molecules to form 1:2, 2:3, 1:3 molecular complexes (possessing non-random structure), respectively, and then change in ΔC_p due to processes II (a)–(b); and III (a)–(c) was given by [54, 55].

$$(\Delta C_p)_{II} = \left[\frac{x_1^2 x_2 ({}^3 \xi_1 / {}^3 \xi_2) \chi_{11}}{x_1 + x_2 ({}^3 \xi_1 / {}^3 \xi_2)} \right] + \left[\frac{x_2^2 x_3 ({}^3 \xi_2 / {}^3 \xi_3) \chi_{22}}{x_2 + x_3 ({}^3 \xi_2 / {}^3 \xi_3)} \right] + \left[\frac{x_3^2 x_1 ({}^3 \xi_3 / {}^3 \xi_1) \chi_{33}}{x_3 + x_1 ({}^3 \xi_3 / {}^3 \xi_1)} \right] \quad (5)$$

$$(\Delta C_p)_{III} = \left[\frac{x_1 x_2 ({}^3 \xi_1 / {}^3 \xi_2) \chi'_{12}}{x_1 + x_2 ({}^3 \xi_1 / {}^3 \xi_2)} \right] + \left[\frac{x_2 x_3 ({}^3 \xi_2 / {}^3 \xi_3) \chi''_{12}}{x_2 + x_3 ({}^3 \xi_2 / {}^3 \xi_3)} \right] + \left[\frac{x_3 x_1 ({}^3 \xi_3 / {}^3 \xi_1) \chi'''_{12}}{x_3 + x_1 ({}^3 \xi_3 / {}^3 \xi_1)} \right] \quad (6)$$

The total change in thermodynamic properties due to processes: I (a)–(c); II (a)–(b); and III (a)–(c) was presented by

$$(C_p^E)_{123} = \sum_{i=I}^{III} (\Delta C_{pi}) = \left[\frac{x_1 x_2 ({}^3 \xi_1 / {}^3 \xi_2)}{x_1 + x_2 ({}^3 \xi_1 / {}^3 \xi_2)} \right] [\chi_{12} + x_1 \chi_{11} + x_2 \chi'_{12}] + \left[\frac{x_2 x_3 ({}^3 \xi_2 / {}^3 \xi_3)}{x_2 + x_3 ({}^3 \xi_2 / {}^3 \xi_3)} \right] [\chi_{23} + x_2 \chi_{22} + x_3 \chi''_{12}] + \left[\frac{x_3 x_1 ({}^3 \xi_3 / {}^3 \xi_1)}{x_3 + x_1 ({}^3 \xi_3 / {}^3 \xi_1)} \right] [\chi_{13} + x_3 \chi_{33} + x_1 \chi'''_{12}] \quad (7)$$

For the present mixtures, it was assumed that (i) interaction parameters for the establishment of unlike contacts 1–2; 2–3_n; 1–3_n are nearly equal to the interaction parameters for the formation of 1:2, 2:3, 1:3 molecular complexes; and (ii) interaction parameters for the rupture

of cohesion forces in (1) or (2) or (3) components are nearly equal then, $\chi_{12} \cong \chi'_{12} = \chi''_{12}$; $\chi_{23} \cong \chi'_{23} = -\chi''_{23}$; $\chi_{13} \cong \chi'_{13} = \chi''_{13}$; $\chi_{11} \cong \chi_{22} \cong \chi_{33} = \chi^*$, Eq. (7) was then expressed as

$$\begin{aligned} (C_P^E)_{123} = & \left[\frac{x_1 x_2 ({}^3\xi_1 / {}^3\xi_2)}{x_1 + x_2 ({}^3\xi_1 / {}^3\xi_2)} \right] [(1 + x_2)\chi_{12}^* + x_1\chi^*] \\ & + \left[\frac{x_2 x_3 ({}^3\xi_2 / {}^3\xi_3)}{x_2 + x_3 ({}^3\xi_2 / {}^3\xi_3)} \right] [(1 + x_3)\chi_{23}^* + x_2\chi^*] \\ & + \left[\frac{x_3 x_1 ({}^3\xi_3 / {}^3\xi_1)}{x_3 + x_1 ({}^3\xi_3 / {}^3\xi_1)} \right] [(1 + x_1)\chi_{13}^* + x_3\chi^*] \end{aligned} \quad (8)$$

Equation (8) contains four unknown parameters: χ_{12}^* , χ_{23}^* , χ_{31}^* and χ^* and these parameters were evaluated by utilizing $(C_P^E)_{123}$ data of the examined mixtures at four arbitrary compositions. The calculated parameters were then used to predict $(C_P^E)_{123}$ values at various values of x_1 and x_2 . Such obtained $(C_P^E)_{123}$ values for the investigated mixtures are presented in Table 3 and also compared with their experimental values. The molar interaction parameters: χ_{12}^* , χ_{23}^* , χ_{31}^* and χ^* evaluated by utilizing $(C_P^E)_{123}$ data for the various mixtures are listed in Table 5. The standard deviations between experimental and calculated values (by Graph theory), $\sigma(C_P^E)_{123}$, are also recorded in Table 5. An examination of Table 3 has revealed that $(C_P^E)_{123}$ values determined by Graph theory compare well their corresponding experimental values which in turn support the various assumptions made in deriving Eq. (8).

Flory's theory

Flory's theory was used to correlate the $(C_P^E)_{123}$ results for the present mixtures which in turn were obtained by differentiating excess molar enthalpies of ternary mixtures with respect to the temperature, T [48, 56, 57]. The theory leads to the following expression for $(C_P^E)_{123}$

$$(C_P^E)_{123} = - \sum_{i=1}^3 \frac{x_i P_1^* \tilde{v}_1^* \alpha_i}{\tilde{v}_1} + \left(\frac{\alpha}{\tilde{v}} \right) \left[\sum_{i=1}^3 x_i P_1^* v_i^* - \sum_{i=1}^3 x_i v_i^* \theta_2 \chi_{12}^{**} \right] \quad (9)$$

where \tilde{v}_1^* , P_1^* , α_i , \tilde{v}_1 and θ_2 ($i = 1$ or 2 or 3) are the characteristic volume, characteristic pressure, thermal coefficient, reduced volume and molecular surface fraction of pure component (1) or (2) or (3) and \tilde{v} , α and χ_{12}^{**} are reduced volume, thermal coefficient and interactional energy parameter of mixture and have the same

significance as described elsewhere [56]. The values of such parameters for pure liquids are also listed in Table 6. The estimation of $(C_P^E)_{123}$ data by Flory theory requires a knowledge of Flory parameters for liquids under investigation along with interaction parameters of (1 + 2), (2 + 3), (1 + 3) binaries which in turn were evaluated by utilizing their H^E values at equimolar composition using equation:

$$H^E = \sum x_i P_1^* (\tilde{U}_1^{-1} - \tilde{U}_{cal}^{-1}) + x_1 v_1^* \theta_2 \chi_{12}^{**} \tilde{U}_{cal}^{-1} \quad (10)$$

where x_i , P_1^* , v_i^* , θ_2 , χ_{12}^{**} , \tilde{U}_1 , and \tilde{U}_{cal} are mole fraction, characteristic pressure, characteristic volume, molecular surface fraction of pure component (1) or (2) or (3), interactional energy parameter of mixture, reduced configurational energy and calculated reduced configurational energy and have the same significance as described elsewhere [58]. Such calculated Flory parameters are listed in Table 6. Benson and D'Arcy [59] further suggested that interaction parameters, χ_{12}^{**} , χ_{23}^{**} , χ_{13}^{**} for (1 + 2), (2 + 3), (1 + 3) binary mixtures must be a function of temperature.

Consequently, $(C_P^E)_{123}$ values were then expressed by

$$\begin{aligned} (C_P^E)_{123} = & - \sum_{i=1}^3 \frac{x_i P_1^* \tilde{v}_1^* \alpha_i}{\tilde{v}_1} + \left(\frac{\alpha}{\tilde{v}} \right) \left[\sum_{i=1}^3 x_i P_1^* v_i^* - \sum_{i=1}^3 x_i v_i^* \theta_2 \chi_{12}^{**} \right] \\ & + \sum_{i=1}^3 \frac{x_i v_i^* \theta_2}{\tilde{v}} \left(\frac{\partial \chi_{12}^{**}}{\partial T} \right) \end{aligned} \quad (11)$$

The reduced volumes, \tilde{v} , and thermal coefficient, α , of ternary mixtures were calculated using

$$\tilde{v} = \left(V_{123}^E + \sum_{i=1}^3 x_i v_i \right) / \sum_{i=1}^3 x_i v_i^* \quad (12)$$

$$\alpha = \sum_{i=1}^3 x_i \alpha_i \quad (13)$$

where V_{123}^E represent excess molar volumes of ternary (1 + 2 + 3) mixtures. The calculated $(C_P^E)_{123}$ values are presented and compared with experimental values in Table 3. Examination of data in Table 3 has revealed that Flory's theory correctly predicts the sign of $(C_P^E)_{123}$ values of [Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures. However, quantitative agreement is poor. The failure of theory to correctly predict the sign of $(C_P^E)_{123}$ data of [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures may be due to strong interactions operating among the various components.

Table 5 Interaction energies: χ_{12}^* , χ_{23}^* , χ_{31}^* and χ^* parameters of Eq. (8) and χ_{12}^{**} , χ_{23}^{**} , χ_{13}^{**} parameters of Flory theory along with connectivity parameters of third degree of a molecule, $({}^3\xi_1)$ or $({}^3\xi_1)_m$ ($1 = 1$ or 2 or 3) utilized in Graph theory for the determination of $(C_p^E)_{123}$ at $T = (293.15\text{--}308.15)$ K

Parameters	T/K			
	293.15	298.15	303.15	308.15
[Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone (3)				
$({}^3\xi_1) = ({}^3\xi_1)_m$	3.403	3.403	3.403	3.403
$({}^3\xi_2) = ({}^3\xi_2)_m$	2.396	2.396	2.396	2.396
$({}^3\xi_3) = ({}^3\xi_3)_m$	1.287	1.287	1.287	1.287
$\chi_{12}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-294.16	-290.48	-288.64	-283.89
$\chi_{23}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-36.82	-37.49	-39.00	-41.51
$\chi_{13}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	54.47	37.65	21.71	8.55
$\chi^*/J\text{ K}^{-1}\text{ mol}^{-1}$	420.80	432.15	446.81	456.32
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Graph)	1.52	1.53	1.40	1.35
$\chi_{12}^{**}/J\text{ cm}^{-3}$	0.90	0.72	0.58	0.55
$\chi_{23}^{**}/J\text{ cm}^{-3}$	-0.10	-0.01	0.14	0.18
$\chi_{13}^{**}/J\text{ cm}^{-3}$	1.78	1.72	1.73	1.73
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Flory)	19.63	19.17	18.67	17.73
[Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclohexanone (3)				
$({}^3\xi_1) = ({}^3\xi_1)_m$	3.403	3.403	3.403	3.403
$({}^3\xi_2) = ({}^3\xi_2)_m$	2.396	2.396	2.396	2.396
$({}^3\xi_3) = ({}^3\xi_3)_m$	2.105	2.105	2.105	2.105
$\chi_{12}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-325.42	-313.10	-298.74	-286.11
$\chi_{23}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	248.97	243.83	234.33	229.39
$\chi_{13}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-14.35	-19.90	-27.02	-28.08
$\chi^*/J\text{ K}^{-1}\text{ mol}^{-1}$	396.59	385.68	378.74	366.30
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Graph)	1.22	1.08	1.18	1.35
$\chi_{12}^{**}/J\text{ cm}^{-3}$	0.90	0.72	0.58	0.55
$\chi_{23}^{**}/J\text{ cm}^{-3}$	0.45	0.58	0.79	0.87
$\chi_{13}^{**}/J\text{ cm}^{-3}$	1.75	1.81	1.99	2.06
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Flory)	18.72	18.23	17.43	16.42
[Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone (3)				
$({}^3\xi_1) = ({}^3\xi_1)_m$	3.403	3.403	3.403	3.403
$({}^3\xi_2) = ({}^3\xi_2)_m$	1.639	1.639	1.639	1.639
$({}^3\xi_3) = ({}^3\xi_3)_m$	1.287	1.287	1.287	1.287
$\chi_{12}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	128.97	143.02	139.75	147.22
$\chi_{23}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	50.44	53.84	58.25	73.60
$\chi_{13}^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-22.95	3.72	7.81	75.18
$\chi^*/J\text{ K}^{-1}\text{ mol}^{-1}$	-142.38	-178.23	-169.62	-219.02
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Graph)	1.64	1.58	1.54	1.52
$\chi_{12}^{**}/J\text{ cm}^{-3}$	0.99	0.90	0.93	0.93
$\chi_{23}^{**}/J\text{ cm}^{-3}$	10.23	10.71	10.51	10.33
$\chi_{13}^{**}/J\text{ cm}^{-3}$	1.78	1.72	1.73	1.73
$\sigma(C_p^E)_{123}/J\text{ K}^{-1}\text{ mol}^{-1}$ (Flory)	25.65	26.94	28.22	31.01
[Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclohexanone (3)				
$({}^3\xi_1) = ({}^3\xi_1)_m$	3.403	3.403	3.403	3.403
$({}^3\xi_2) = ({}^3\xi_2)_m$	1.639	1.639	1.639	1.639
$({}^3\xi_3) = ({}^3\xi_3)_m$	2.105	2.105	2.105	2.105

Table 5 continued

Parameters	T/K			
	293.15	298.15	303.15	308.15
$\chi_{12}^*/J\ K^{-1}\ mol^{-1}$	28.91	34.94	38.94	46.21
$\chi_{23}^*/J\ K^{-1}\ mol^{-1}$	114.06	118.12	121.23	115.53
$\chi_{13}^*/J\ K^{-1}\ mol^{-1}$	-43.18	-43.22	-40.37	-27.11
$\chi^*/J\ K^{-1}\ mol^{-1}$	10.22	4.18	-0.64	-17.64
$\sigma(C_P^E)_{123}/J\ K^{-1}\ mol^{-1}$ (Graph)	1.23	1.20	1.13	0.94
$\chi_{12}^{**}/J\ cm^{-3}$	0.99	0.90	0.93	0.93
$\chi_{23}^{**}/J\ cm^{-3}$	4.53	4.98	5.44	5.20
$\chi_{13}^{**}/J\ cm^{-3}$	1.75	1.81	1.99	2.06
$\sigma(C_P^E)_{123}/J\ K^{-1}\ mol^{-1}$ (Flory)	15.56	16.65	18.12	18.74

Also included are the deviations, $\sigma(C_P^E)_{123}$, between experimental and calculated $(C_P^E)_{123}$ values by investigated theories

Table 6 Parameters of pure components, Characteristic volume, V^* , characteristic pressure, P^* , molar volume, V , reduced volume, \tilde{v} and thermal expansion coefficient, α , used in Flory theory calculations at $T = (293.15\text{--}308.15)\ K$

Components	T/K	$V^*/cm^3\ mol^{-1}$	$P^*/J\ cm^{-3}$	$V/cm^3\ mol^{-1}$	$\tilde{v}/cm^3\ mol^{-1}$	$\alpha(\times 10^{-3})/K^{-1}$
<i>1-butyl-2,3-dimethyl imidazolium tetrafluoroborate</i>	293.15	185.73	324.67	201.13	1.08	0.299
	298.15	184.76	351.26	201.42	1.09	0.322
	303.15	184.51	360.43	201.78	1.09	0.329
	308.15	184.23	369.48	202.08	1.10	0.336
<i>1-butyl-3-methyl imidazolium tetrafluoroborate</i>	293.15	159.60	687.93	187.86	1.18	0.687
	298.15	160.95	656.03	188.52	1.17	0.650
	303.15	162.68	611.45	189.08	1.16	0.601
	308.15	163.11	605.63	189.66	1.16	0.594
<i>1-ethyl-3-methyl imidazolium tetrafluoroborate</i>	293.15	132.84	689.00	153.98	1.16	0.609
	298.15	133.31	678.42	154.46	1.16	0.596
	303.15	132.93	700.33	154.91	1.17	0.614
	308.15	132.87	711.48	155.42	1.17	0.622
<i>Cyclopentanone</i>	293.15	71.03	660.42	88.61	1.25	1.016
	298.15	71.12	659.21	89.06	1.25	1.022
	303.15	71.20	658.06	89.52	1.26	1.030
	308.15	71.32	655.39	89.98	1.26	1.034
<i>Cyclohexanone</i>	293.15	83.90	633.81	103.59	1.23	0.953
	298.15	83.59	652.20	104.08	1.25	0.987
	303.15	83.13	675.54	104.62	1.26	1.036
	308.15	83.05	682.33	105.17	1.27	1.056

Conclusions

Excess heat capacities, $(C_P^E)_{123}$, of ternary ionic liquid mixtures of [Bmmim][BF₄] (1) + [Bmim][BF₄] or [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) have been determined by utilizing the measured molar heat capacities $(C_P)_{123}$ data of the said mixtures at the studied temperatures. While $(C_P^E)_{123}$ values of [Bmmim][BF₄] (1) + [Emim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures are

positive over the entire mole fraction of components (1) and (2), those for [Bmmim][BF₄] (1) + [Bmim][BF₄] (2) + cyclopentanone or cyclohexanone (3) mixtures change sign with change in relative proportion of constituent molecules. The analysis of $(C_P^E)_{123}$ data suggests that cyclohexanone gives relatively more compact structure in [Bmmim][BF₄]: [Bmim][BF₄] and [Bmmim][BF₄]: [Emim][BF₄] molecular entities as compared to cyclopentanone. The $(C_P^E)_{123}$ data have also been analyzed in terms of (i) Graph; and (ii) Flory

theories. It has been observed that values predicted by Graph theory compare well with their experimental values. However, Flory theory shows only qualitative agreement with measured values.

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